

Status of International Standardization on CO₂Transportation

ISO 27913 / TC 265 Carbon dioxide capture, transportation, and
geological storage – Pipeline transportation systems



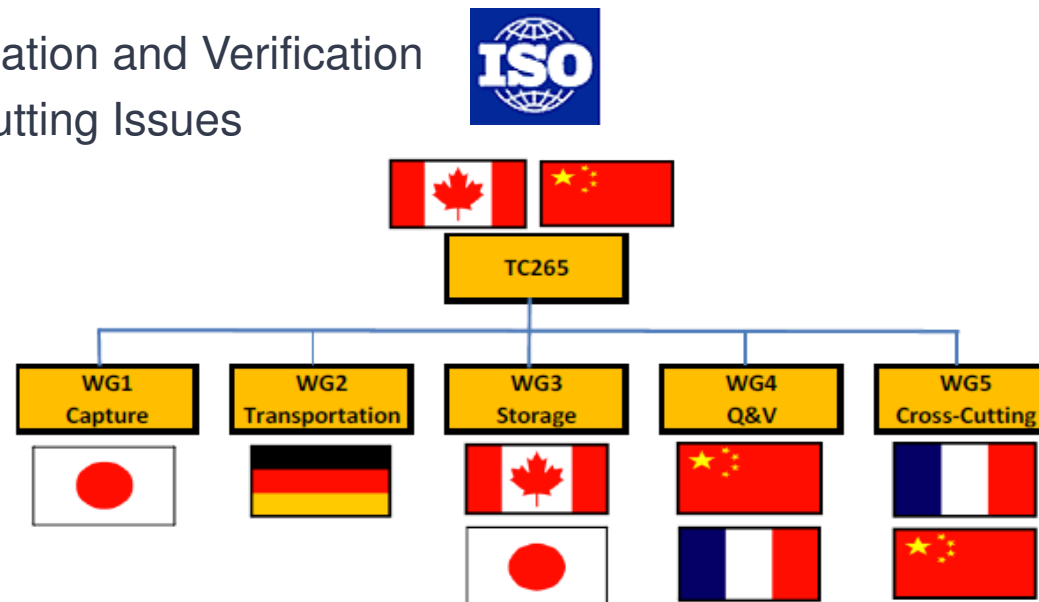
Content

- History
- Status
- CO₂ – Specific Main Issues
 - Boundaries to Capture and Storage
 - Fracture arrest
 - Corrosion
 - Non-discriminatory transportation

History of ISO TC 265

2011 June:

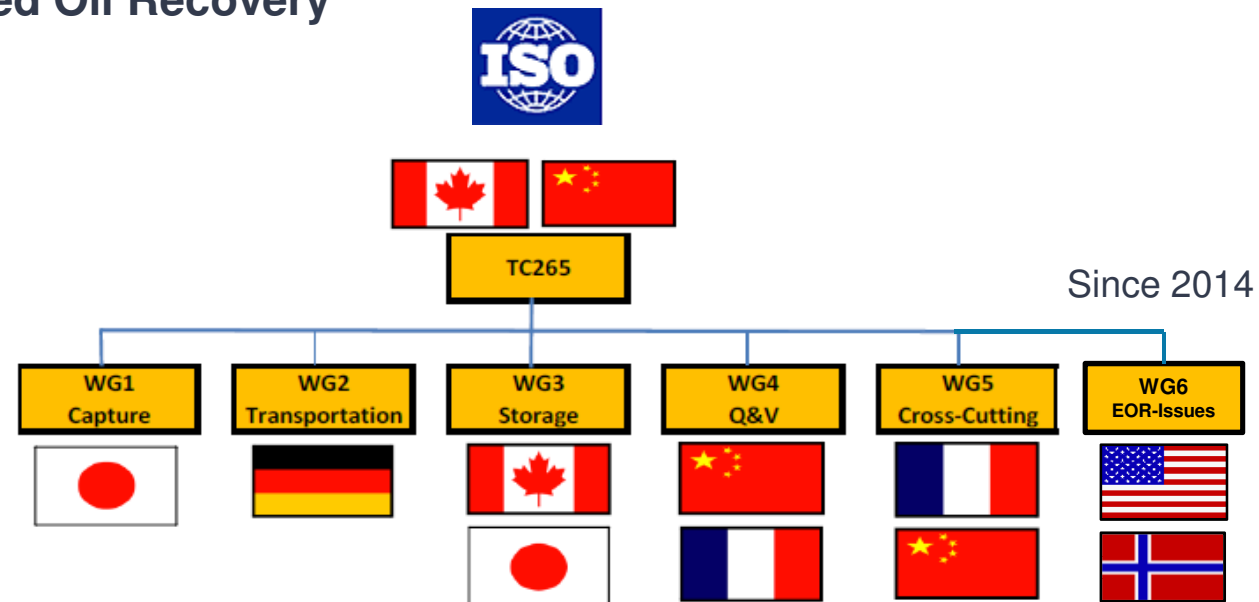
- Foundation of the ISO Technical Committee (TC) 265 for Carbon dioxide capture, transportation, and geological storage in Paris:
 - WG 1 Capture
 - WG 2 Transportation
 - WG 3 Storage
 - WG 4 Quantification and Verification
 - WG 5 Cross-Cutting Issues



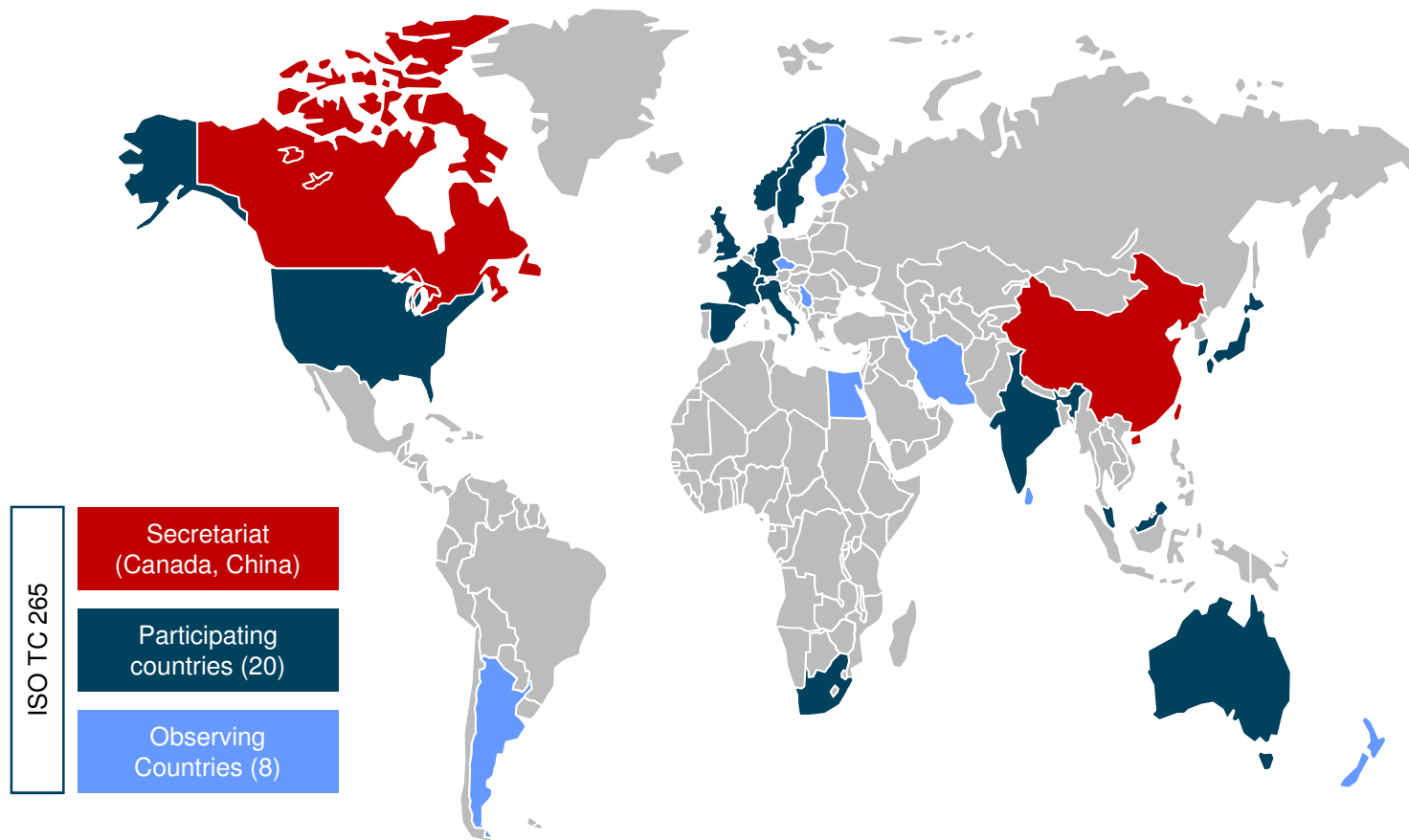
History of ISO TC 265

Today:

- WG 1 Capture
- WG 2 Transportation
- WG 3 Storage
- WG 4 Quantification and Verification
- WG 5 Cross-Cutting Issues
- **WG 6 Enhanced Oil Recovery**

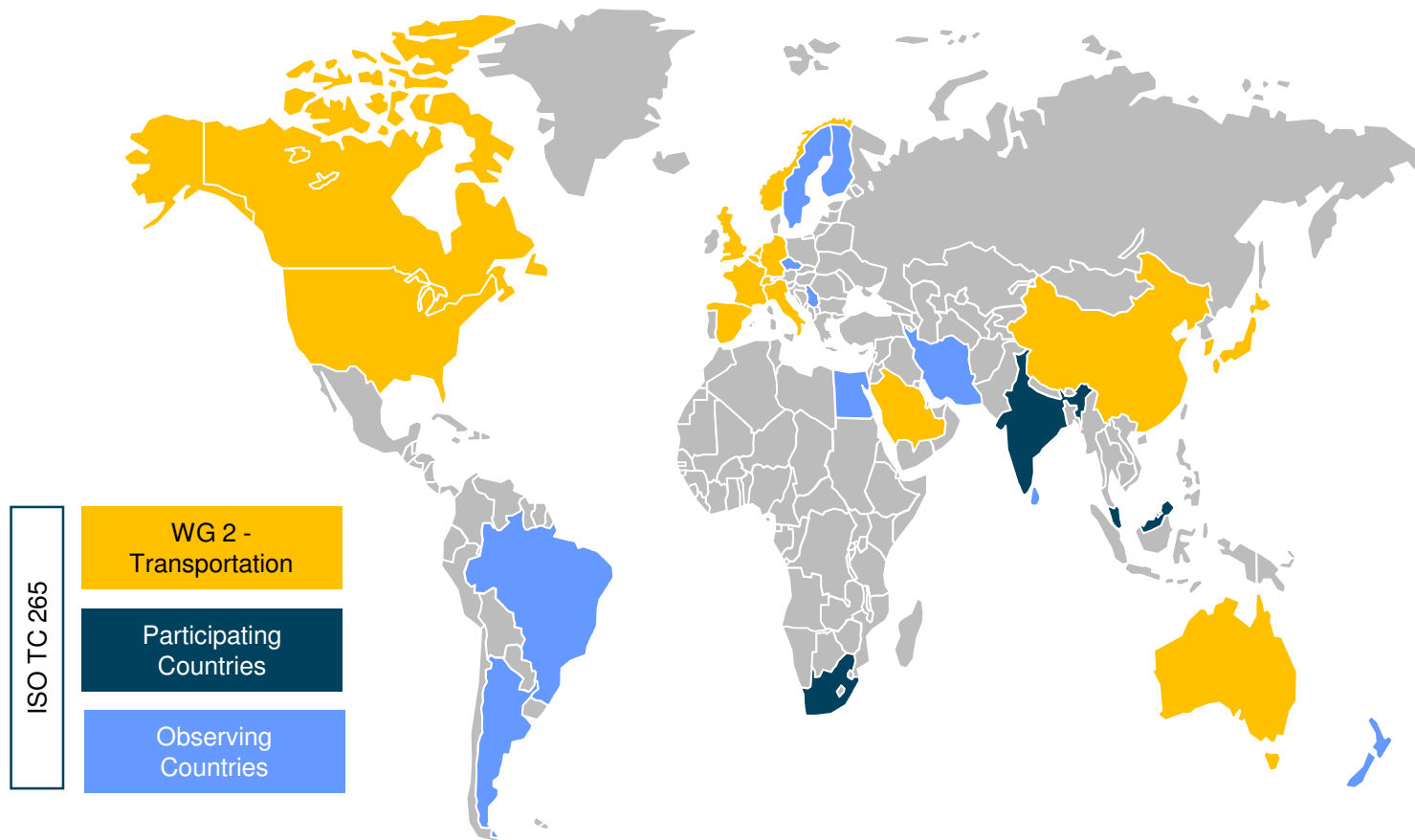


ISO/TC 265 Members



WG 2: Members of Working Group CO₂ Transportation

Total members: 50



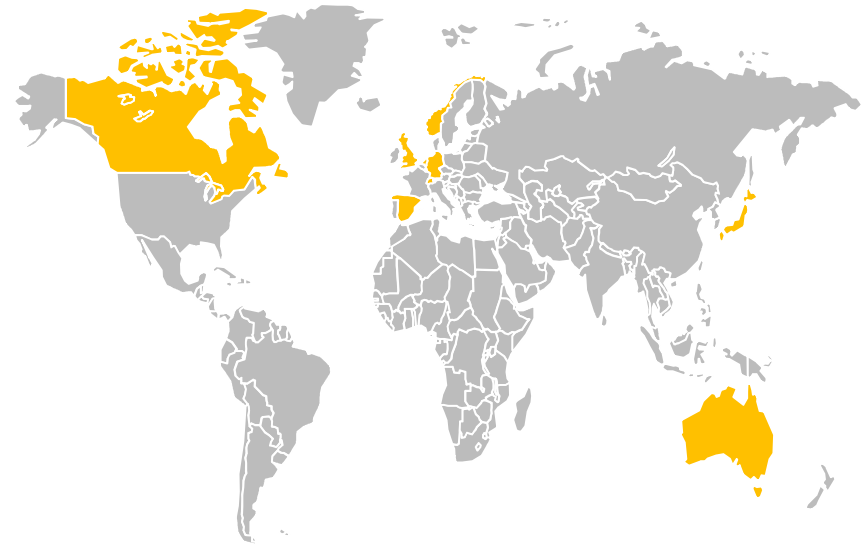
WG 2 Meetings History

2013

ISO/TC 265/WG2

1st: 2013-06 Bonn, Germany, DVGW:

- Collect CCS-know-how
- Discuss available standards and needs for CO₂
- Develop strategy
- Take DNV RP-J202 as a starting basis
- Distribute work to experts around the world to derive a first **Working Draft (WD)**: **active participants in orange**
- Define Responsible Persons for WD Revision:
 - **Australia:** Michael Malavazos
 - **Canada:** Brian Rothwell
 - **Germany:** Sven Anders, Claudia Werner
 - **Norway:** Jock Brown
 - **UK:** Andy Brown



WG 2 Meetings History

2014

ISO/TC 265/WG2

2nd :2014-02 London, UK, BSI:

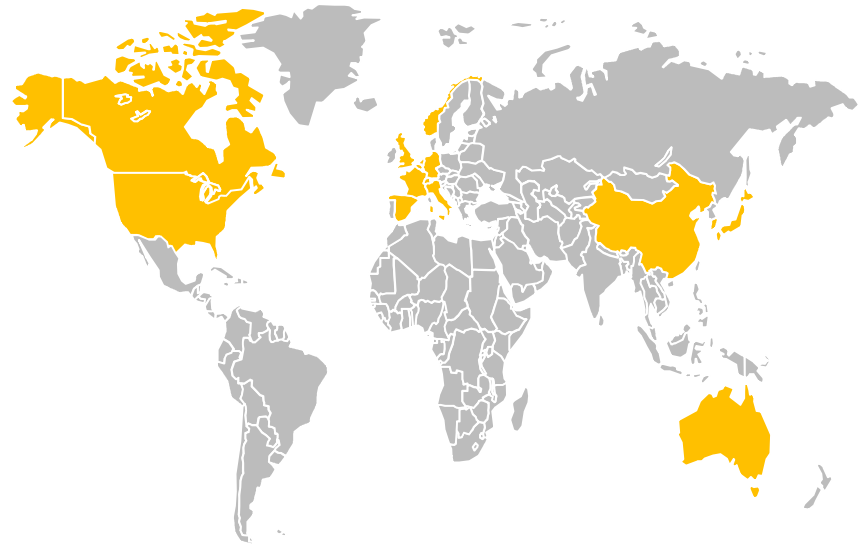
- Work on **Working Draft**
- Main topics: Fracture arrest assurance, corrosion, CO₂-composition

3rd: 2014-04 Berlin, Germany, DIN:

- Finalize Working Draft (WD)
- China and USA joined WG2 meeting
- Distribute Working Draft (WD) for comments inside WG2

4th: 2014-08 Gelsenkirchen, Germany, E.ON:

- Discussion and solution of comments on WD
- Prepare to submit **Committee Draft (CD)** for comments in September



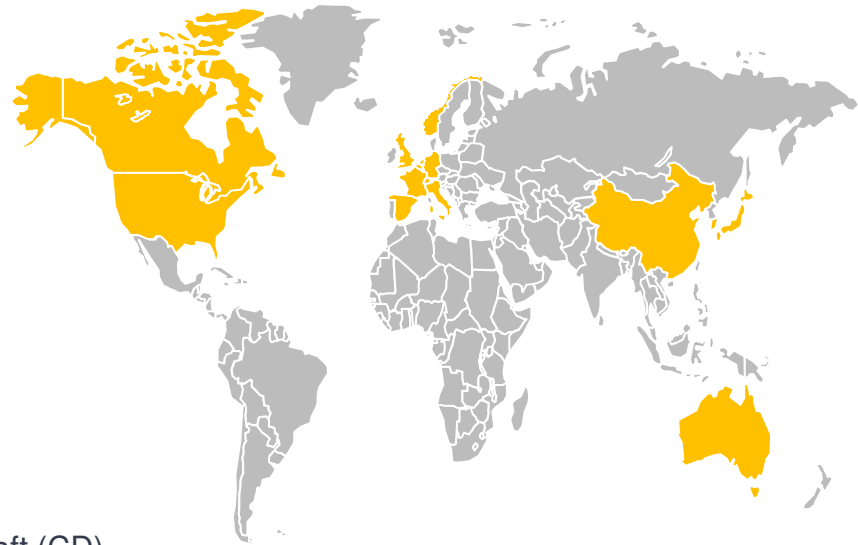
WG 2 Meetings History

2015

ISO/TC 265/WG2

5th: 2015-01 Birmingham, USA, ANSI:

- Discussion and solution of 427 comments on Committee Draft (CD)
- Provision of **Draft International Standard (DIS)** (ISO/DIS 27913 CO₂-Transportation) in March 2015 for DIS Ballot (until October 2015)

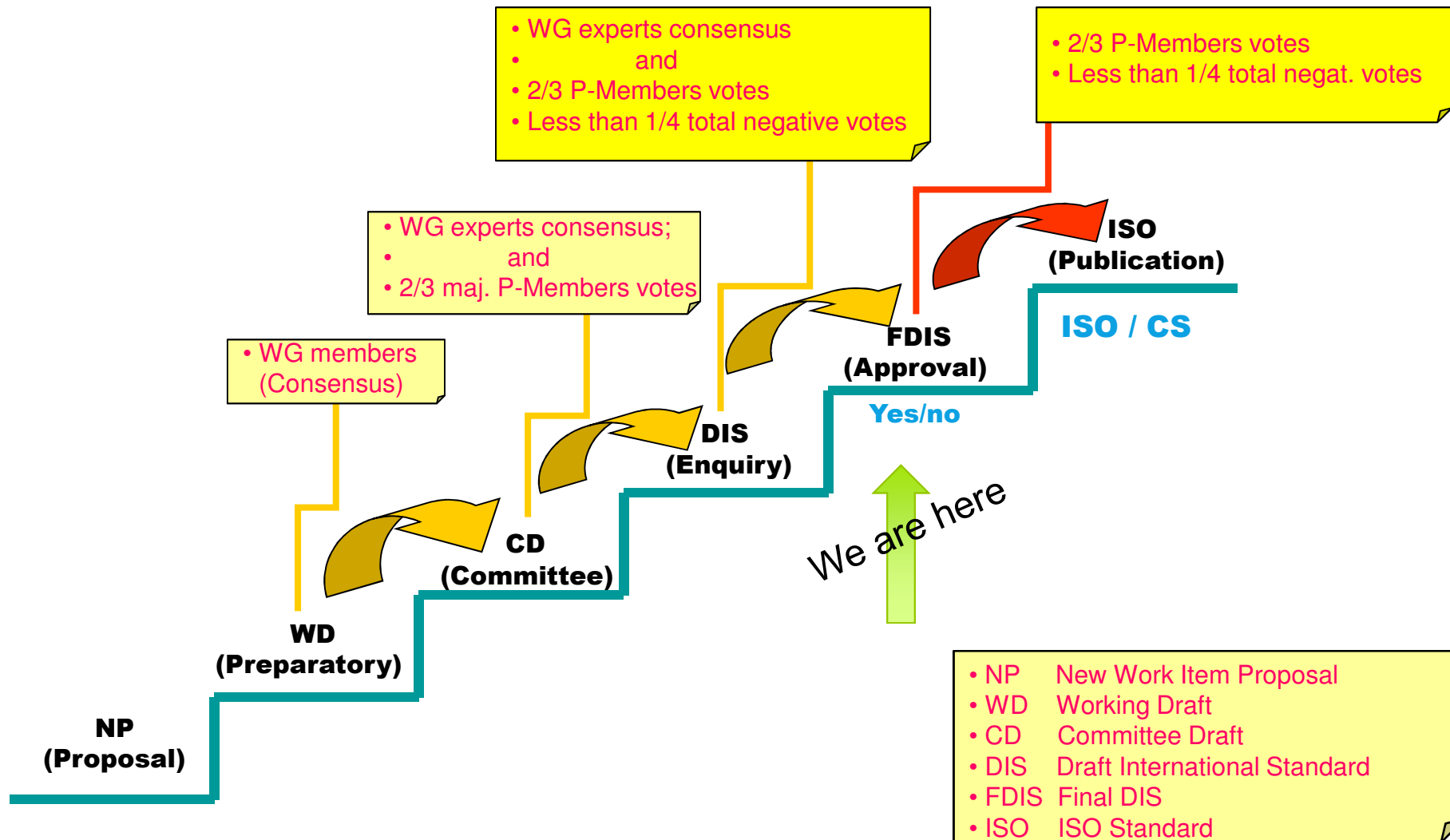


6th: 2015-12 Kjeller near Oslo, Norway, IFE:

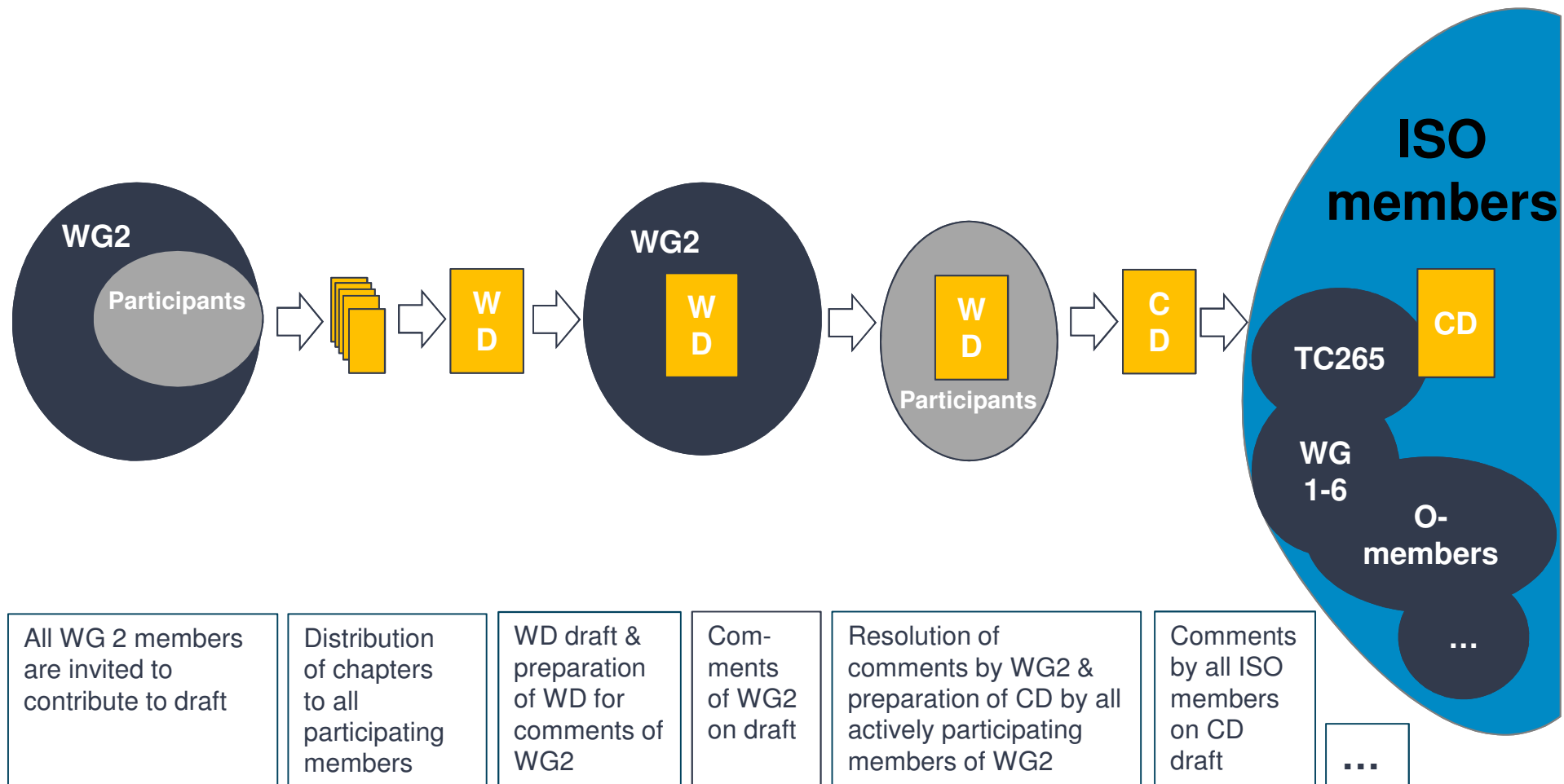
- Discussion and solution of 216 comments on DIS
- Provision of ISO 27913



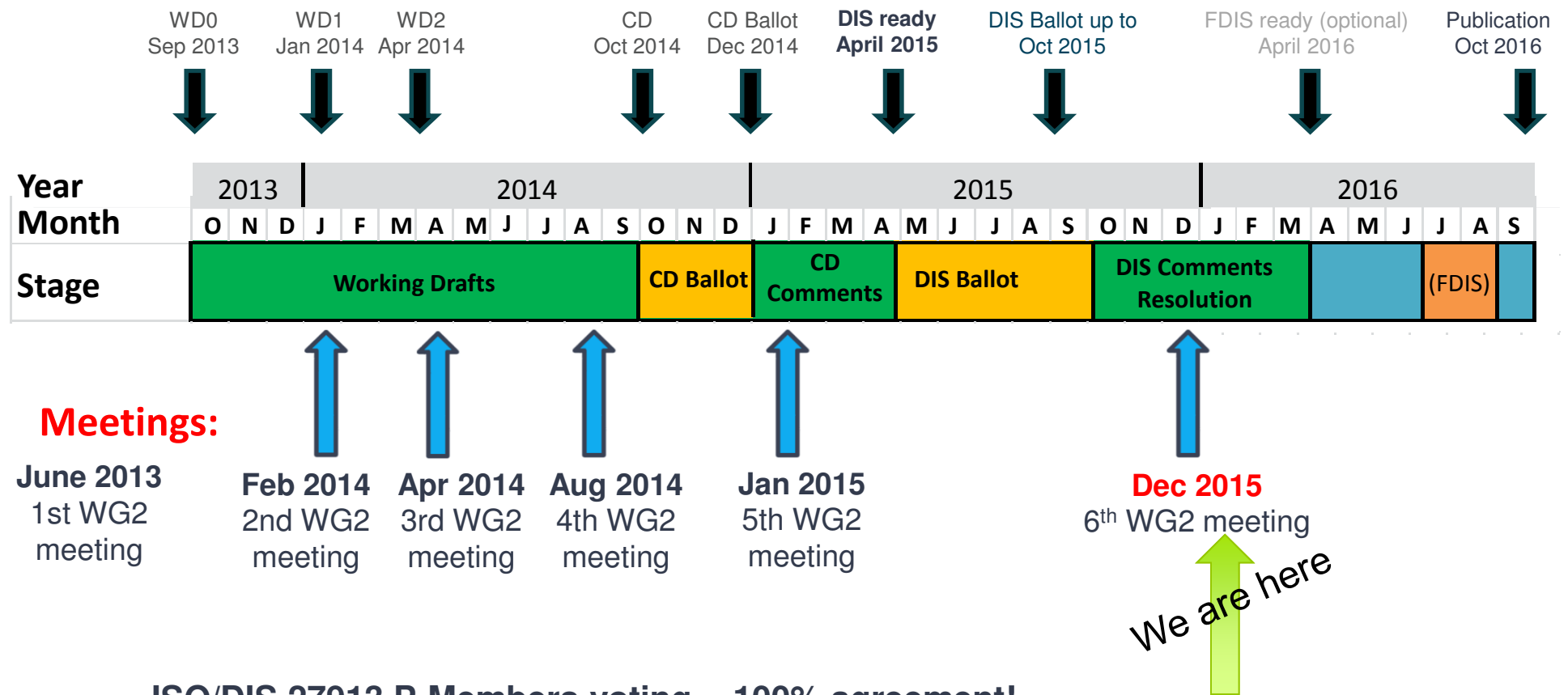
ISO Standards Development



Worldwide participation at all stages of development



Timeline



ISO/DIS 27913 P-Members voting = 100% agreement!

Content of the Standard ISO 27913

ISO/TC 265/SC

Date: 2015-12-03

ISO/DIS 27913

ISO/TC 265/SC /WG 2

Secretariat: SCC

Carbon dioxide capture, transportation and geological storage — Pipeline transportation systems

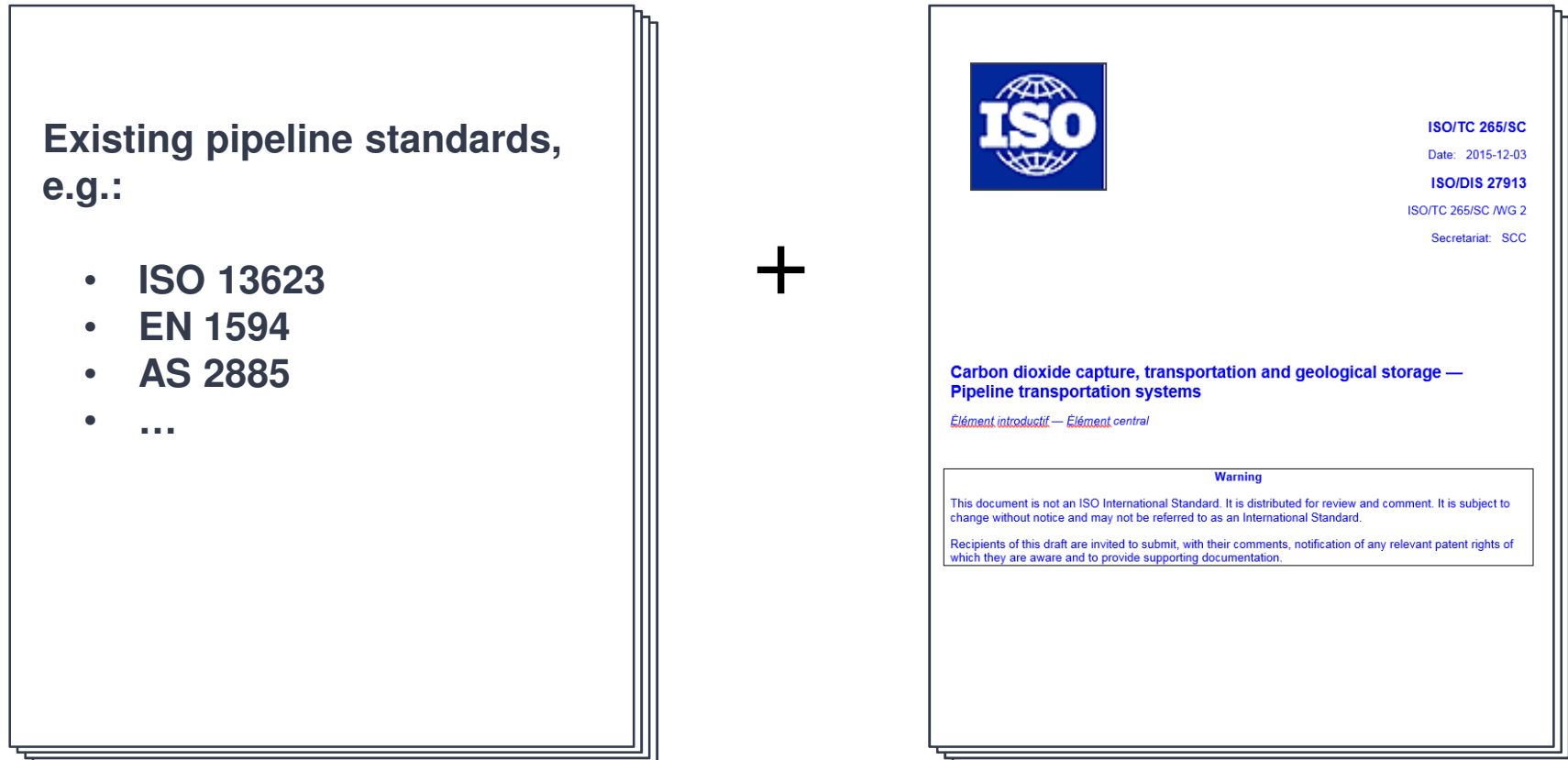
Élément introductif — Élément central

Warning

This document is not an ISO International Standard. It is distributed for review and comment. It is subject to change without notice and may not be referred to as an International Standard.

Recipients of this draft are invited to submit, with their comments, notification of any relevant patent rights of which they are aware and to provide supporting documentation.

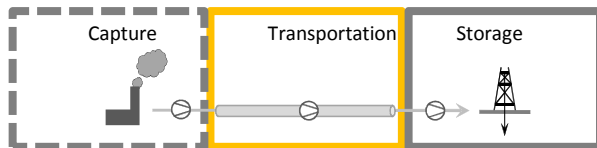
Basis for ISO 27913 Pipeline transportation systems



This new ISO 27913 contains **additional CO₂ specific requirements and recommendations** not covered in existing pipeline standards.

CO₂ – Specific Main Issues

Boundaries to Capture and Storage



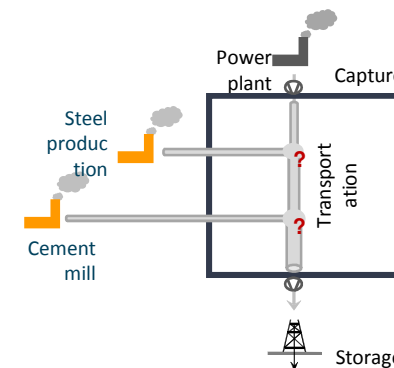
Fracture arrest



Corrosion

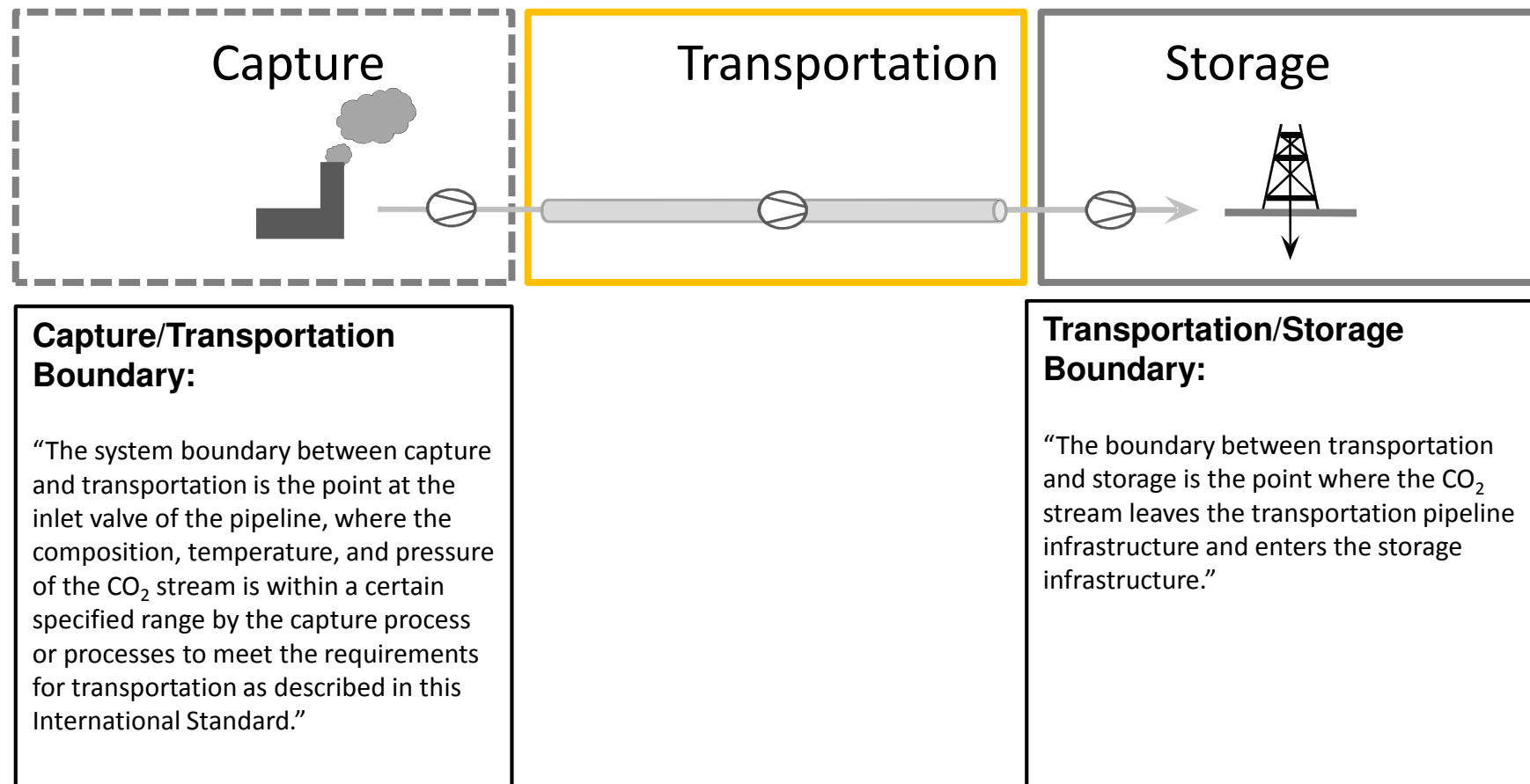


Non-discriminatory transportation



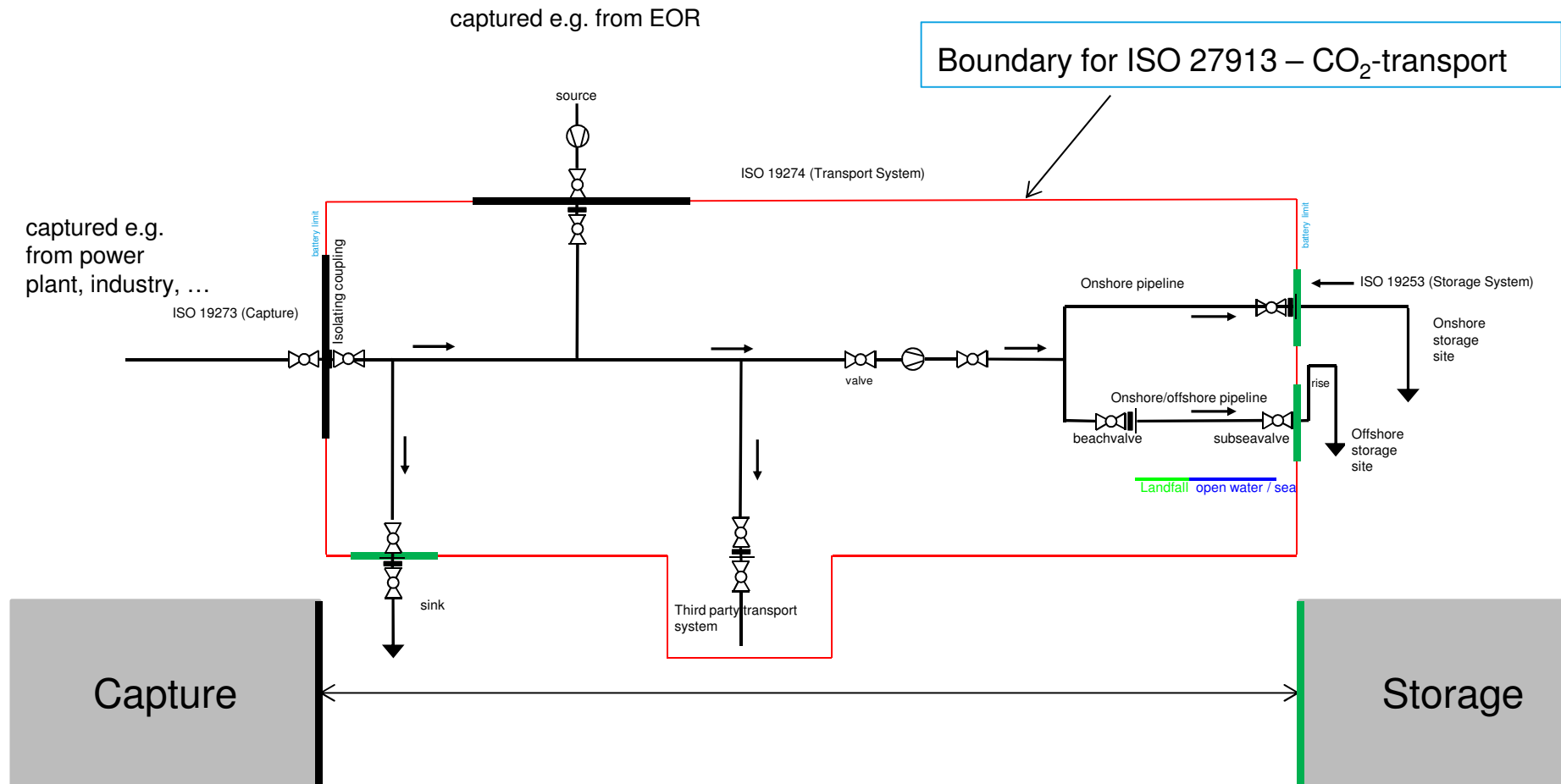
CO₂ – Specific Main Issues

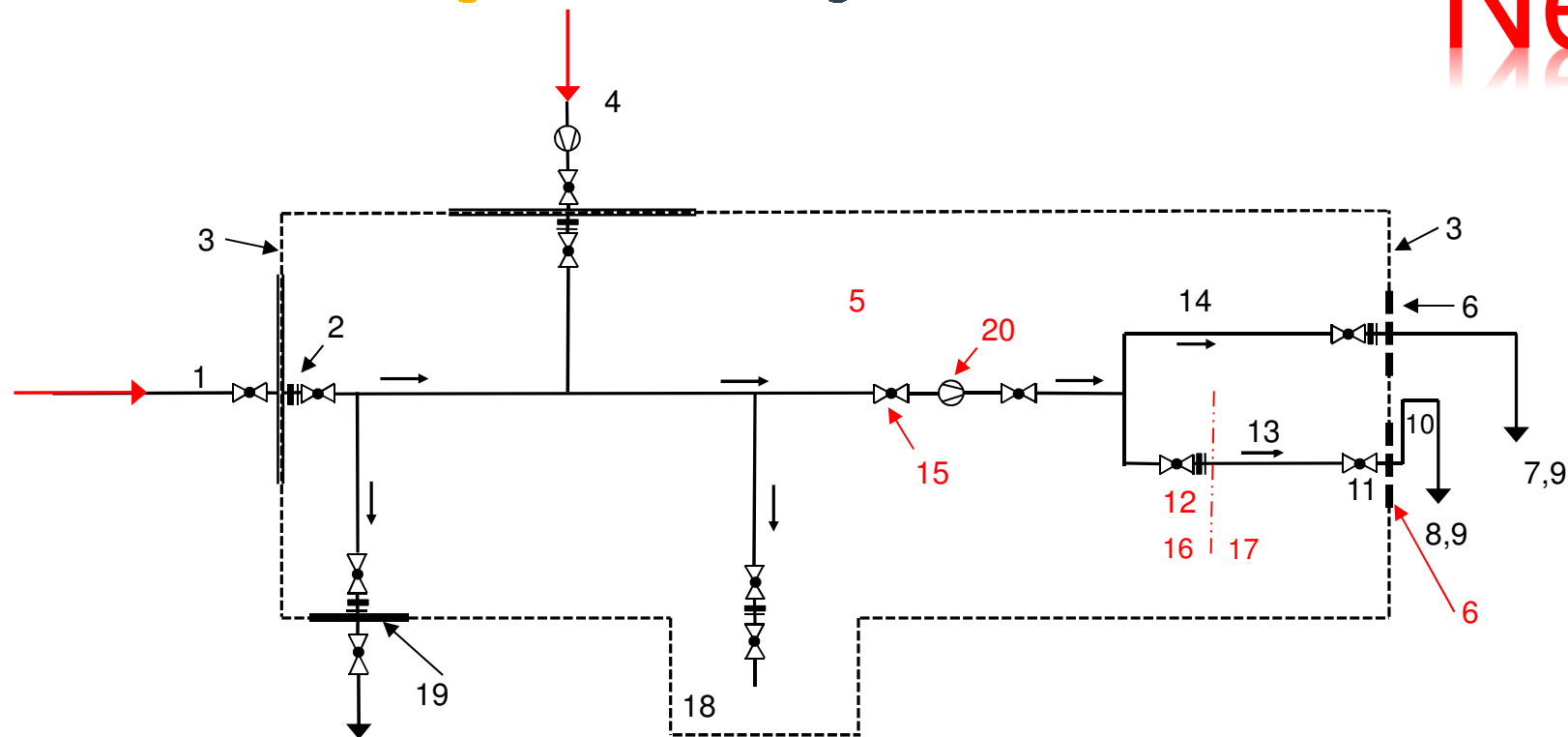
CCS System boundaries 1



Source: ISO/DIS 27913

Definition of CO₂ Transport Boundaries





- Key**
- | | | | |
|---|---|----|---------------------------------------|
| 1 | capture e.g. from power plant, industry, ... , see ISO/AWI TR 27912 (capture) | 10 | Riser (out of transport scope) |
| 2 | isolating joint | 11 | Subsea valve (Inside transport scope) |
| 3 | boundary limit | 12 | Beach valve |
| 4 | source other source of CO ₂ | 13 | Onshore/offshore pipeline |
| 5 | ISO/AWI 27913 (transportation system inside) | 14 | Onshore pipeline |
| 6 | ISO/AWI 27914 (storage system) | 15 | Valve |
| 7 | Onshore storage site | 16 | Landfall |
| 8 | Offshore storage site | 17 | Open water/sea |
| 9 | ISO/AWI 27916 (EOR) | 18 | Third party transport system |
| | | 19 | Export to other uses than 7, 8 and 9 |
| | | 20 | Intermediate compression or pumping |
| | | 21 | Isolation joint |

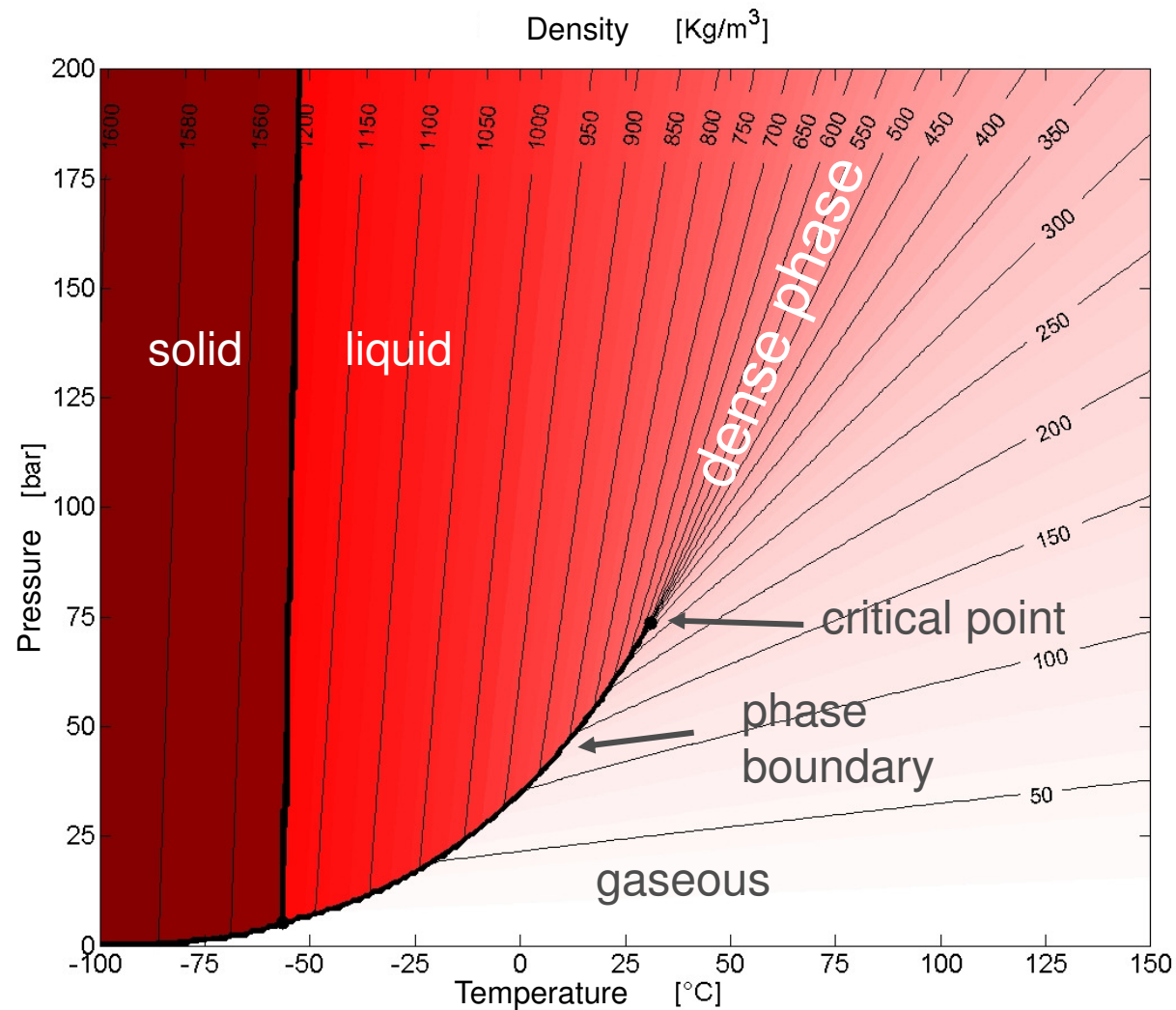
Figure 1 — Schematic illustration of the system boundaries of ISO 27913

CO₂ – Specific Main Issues

Fracture Arrest

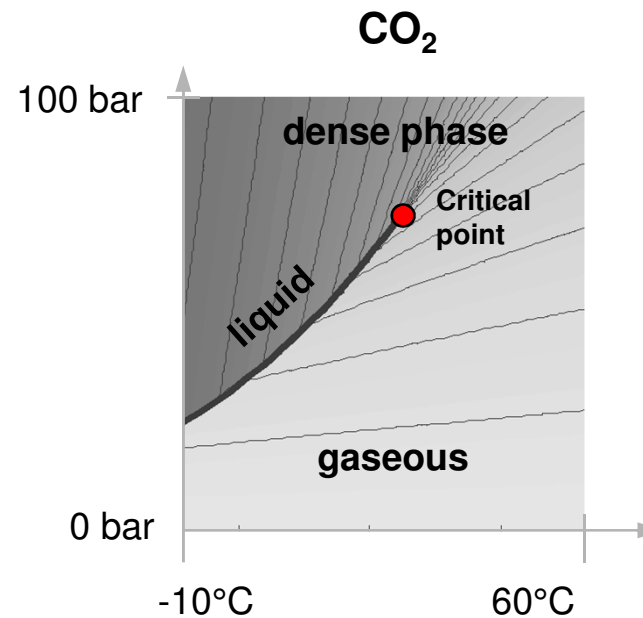


Thermodynamic properties: Pure CO₂



Differences CO₂ versus natural gas

- Phase behavior
(three different phases, depended on purity)
- Liquid and dense phase may result in hydraulic shocks
- Fracture propagation / arrest
- ...



Fracture propagation is a NO!-GO!

- Ductile / brittle fracture → crack
- Joule-Thomson effect promotes embrittlement
- CO₂ decompression behaviour promotes crack propagation

Countermeasures:

- Use of special steels
- Increased wall thickness
- Fiberglass-reinforced plastic cuffs (fracture arrestors)

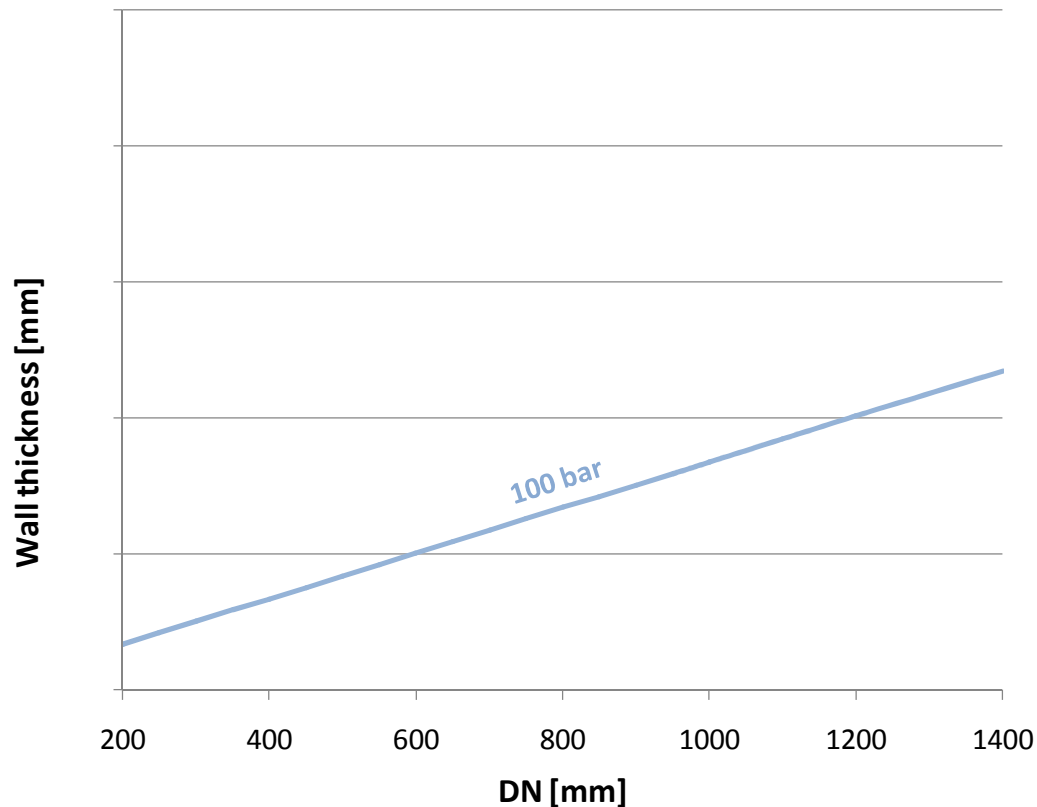
fracture
arrest



fracture
propagation



Wall thickness against internal pressure



$$T_{minDP} = \frac{DP \cdot DN}{20 \cdot f_0 \cdot R_{t0.5}}$$

T_{minDP} : Minimum wall thickness
against internal pressure [mm]

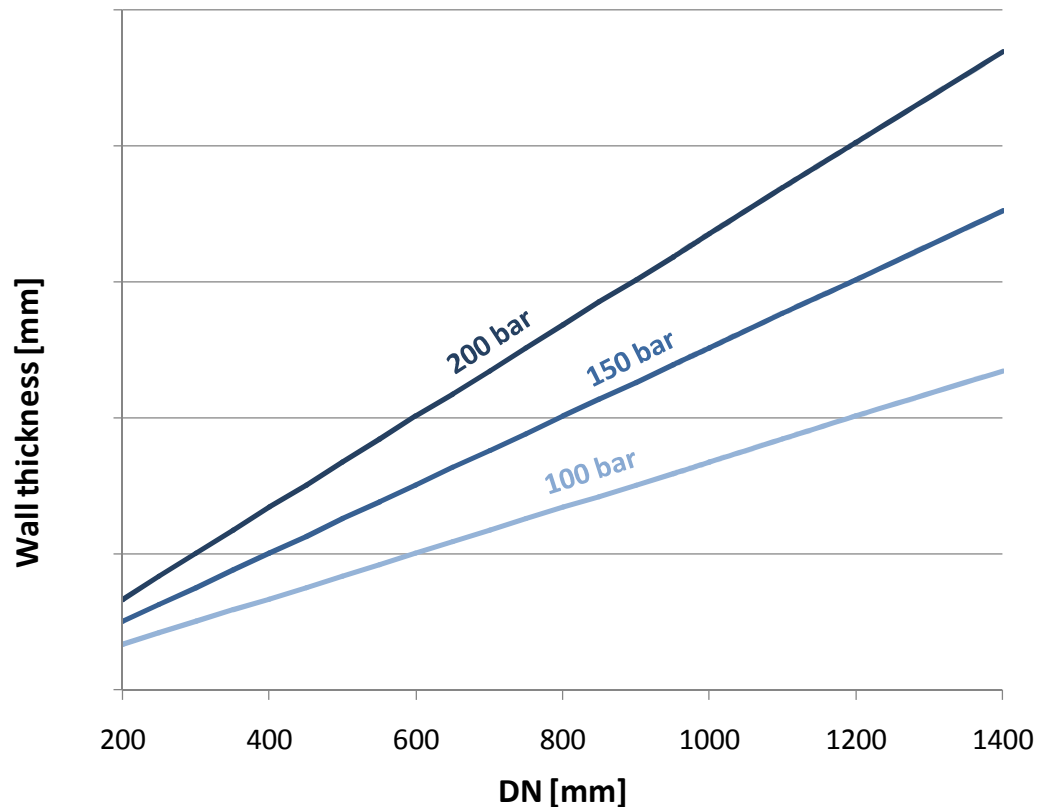
DP: Design Pressure [bar]

DN: Nominal Diameter [mm]

f_0 : Load factor [-]

$R_{t0.5}$: Specified minimum yield
strength [N/mm²]

Wall thickness against internal pressure



$$T_{minDP} = \frac{DP \cdot DN}{20 \cdot f_0 \cdot R_{t0.5}}$$

T_{minDP} : Minimum wall thickness
against internal pressure [mm]

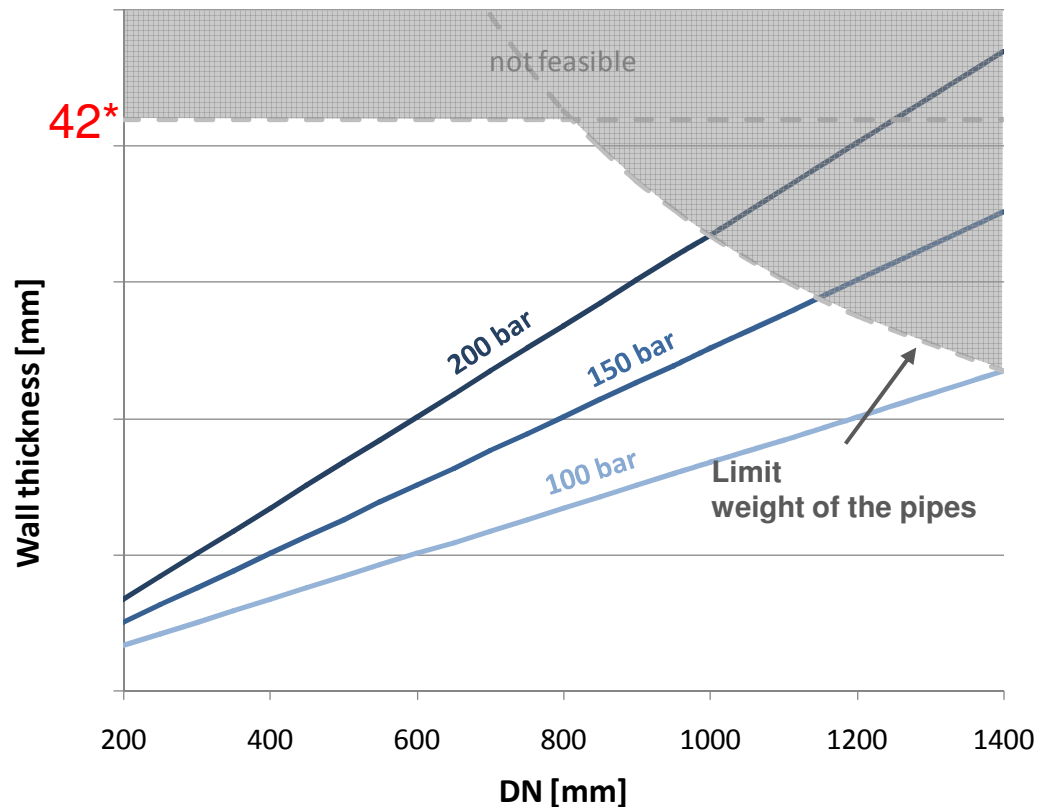
DP: Design Pressure [bar]

DN: Nominal Diameter [mm]

f_0 : Load factor [-]

$R_{t0.5}$: Specified minimum yield
strength [N/mm²]

Wall thickness against internal pressure



$$T_{minDP} = \frac{DP \cdot DN}{20 \cdot f_0 \cdot R_{t0.5}}$$

T_{minDP} : Minimum wall thickness against internal pressure [mm]

DP: Design Pressure [bar]

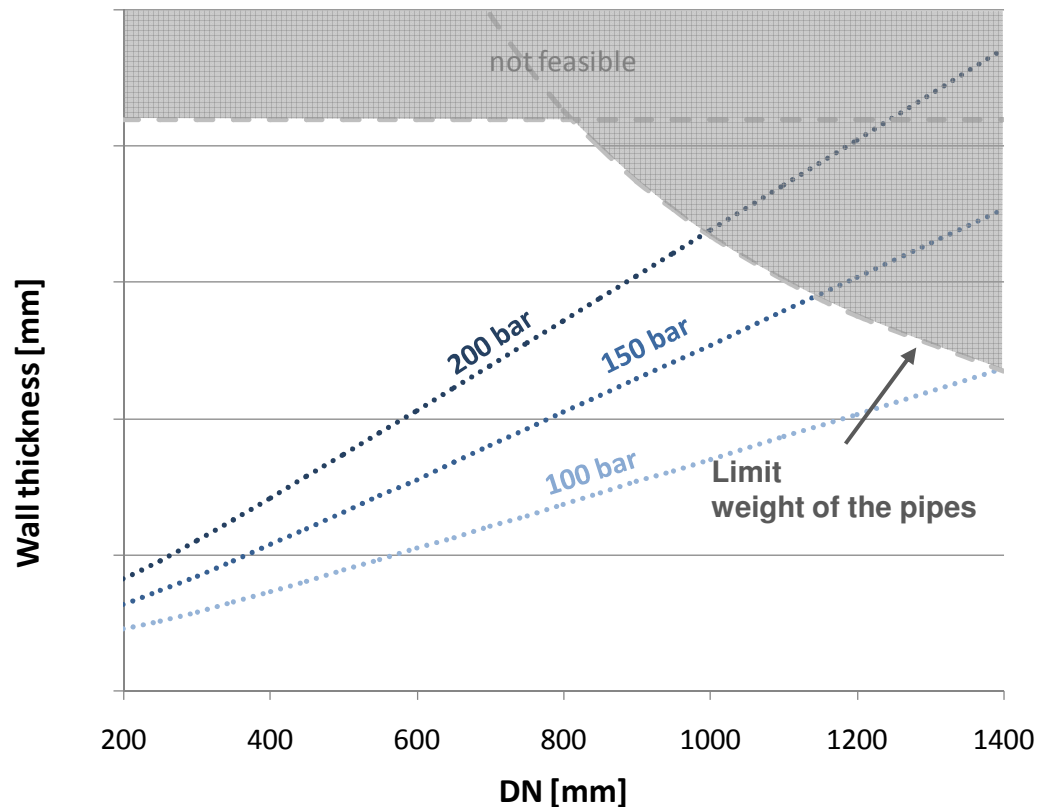
DN: Nominal Diameter [mm]

f_0 : Load factor [-]

$R_{t0.5}$: Specified minimum yield strength [N/mm²]

* The number 42 is, in The Hitchhiker's Guide to the Galaxy by Douglas Adams, "The Answer to the Ultimate Question of Life, the Universe, and Everything"

Wall thickness against internal pressure and hydraulic shock



$$\Delta p_{Jou} = \rho \cdot a \cdot \Delta v \cdot 10^{-5}$$

Δp_{Jou} : Change in pressure [bar]

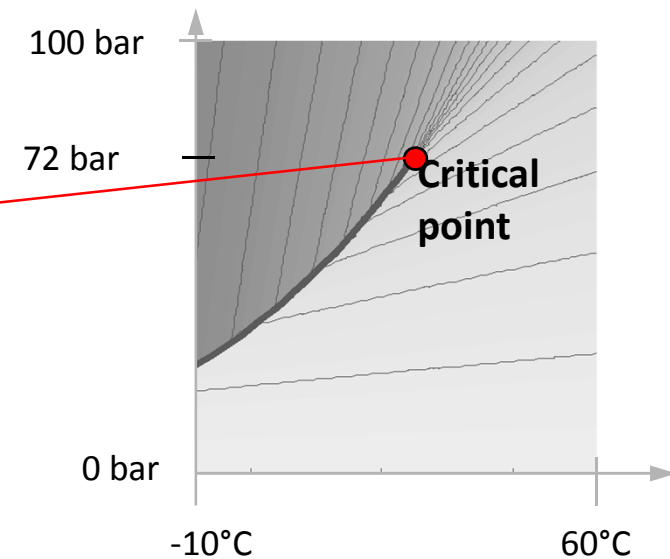
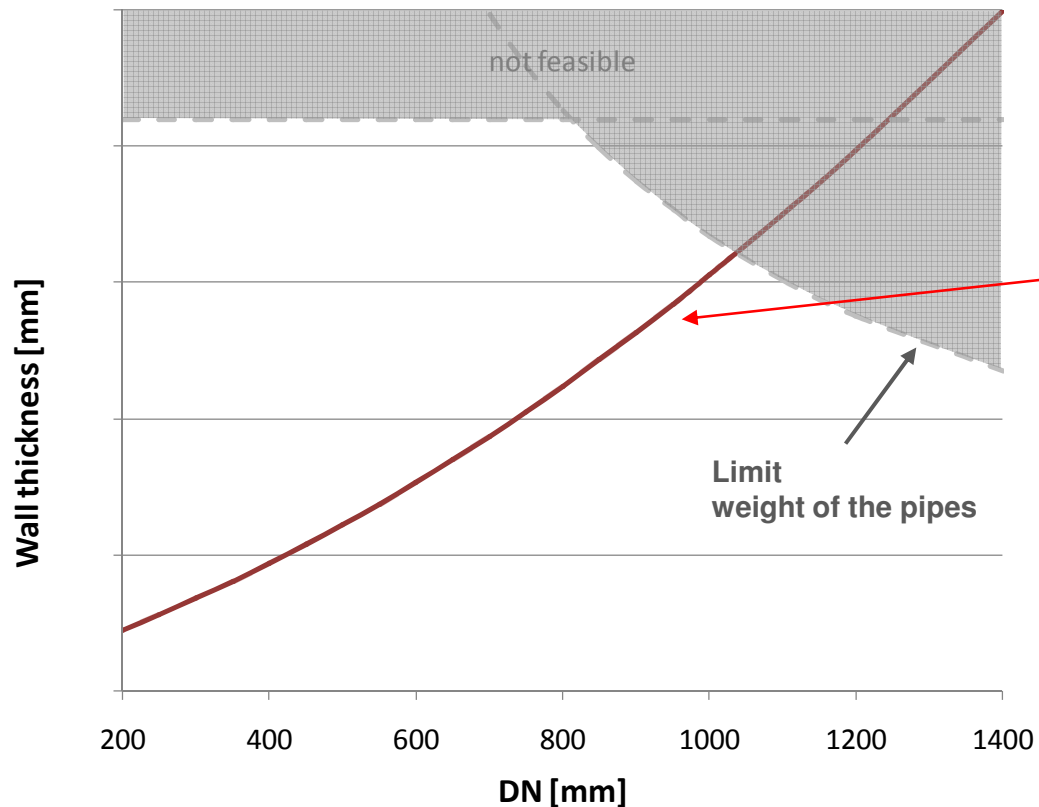
ρ : Density [bar]

a : Wave propagation velocity [m/s]

Δv : Change in velocity [m/s]

Wall thickness for crack-arrest

$$\frac{C_v E}{A_c \bar{\sigma}^2 \sqrt{Rt}} = \frac{24}{\pi} \ln \sec \left[\frac{\pi}{2} \cdot \frac{3.33 \sigma_a}{\bar{\sigma}} \right]$$



Parameters: Steel X 70, $C_v > 100$ J
Driving pressure at critical point

Modified Battelle-Two-Curve

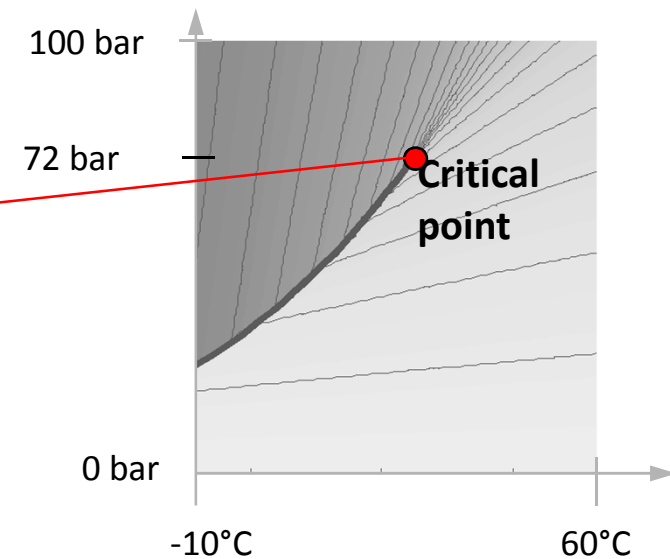
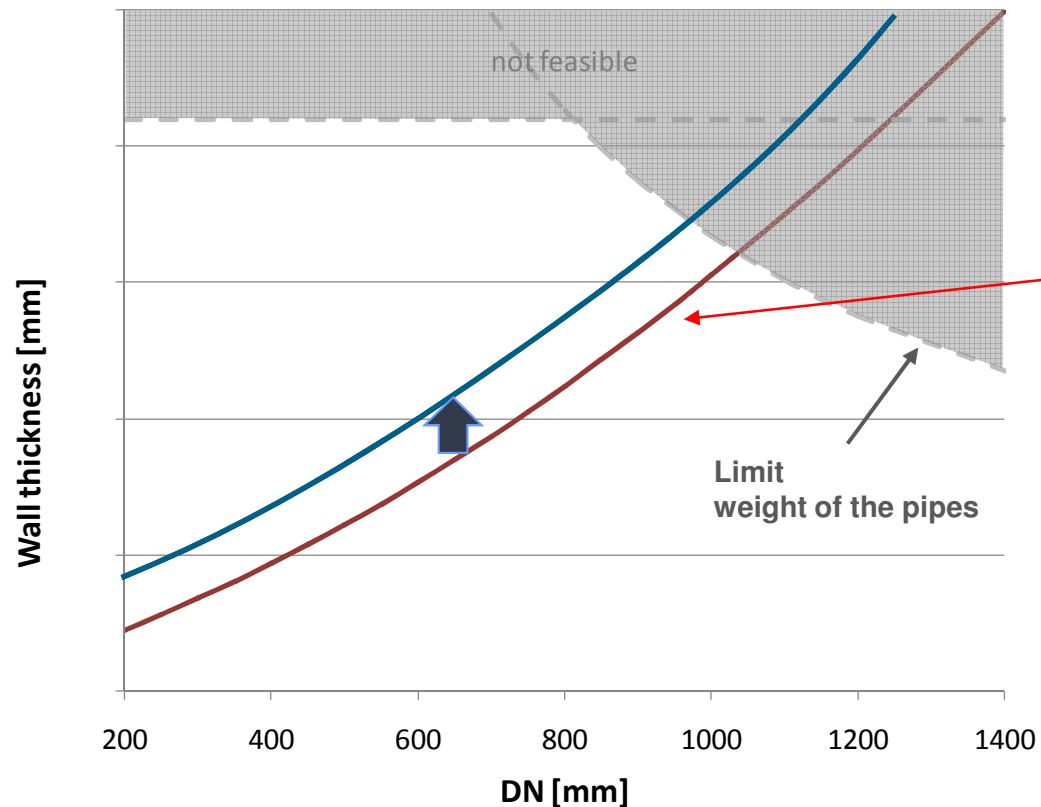
One approach to calculate the wall thickness against ductile fracture is the use of the standard Battelle Two-Curve approach. The Battelle Two Curve Model was originally derived from decompression tests using lean and rich gasses, which exhibited no plateau or a short plateau: since the decompression curve for CO₂ has a very long plateau, the Battelle-Two-Curve-Model has not been shown to be sufficiently conservative for CO₂ under some conditions [20]. These conditions particularly exist if a Charpy-V-notch toughness of > 100 Joule is required. However, because the relationship between Charpy V-notch impact energy and the ductile fracture propagation resistance of the steel is not linear, there is some additional uncertainty in the application of the Charpy V-notch test alone when the arrest toughness is very high (>330J), [20].

For line pipe material with Charpy-V-notch toughness < 330 J, and until additional test results permit a comprehensive mathematical solution, a suggested approach is to apply an additional correction factor to the relevant hoop stress. Based on the current knowledge a correction factor of $c_{cf} \geq 1,2$ is recommended unless it can be demonstrated otherwise. Specialist advice can be obtained to determine an alternative correction factor $c_{cf} \geq 1$.

$$1000 \frac{C_v \cdot E}{A_c \cdot \sigma_f^2 \cdot \sqrt{R \cdot t}} = \frac{24}{\pi} \cdot \ln \left(\sec \left[\frac{\pi}{2} \cdot \frac{c_{cf} \cdot 3,33 \cdot \sigma_a}{\sigma_f} \right] \right) \quad (1)$$

Wall thickness for crack-arrest

$$\frac{C_v E}{A_c \bar{\sigma}^2 \sqrt{Rt}} = \frac{24}{\pi} \ln \sec \left[\frac{\pi^{1,2} 3.33 \sigma_a}{2 \cdot \frac{\sigma}{\bar{\sigma}}} \right]$$



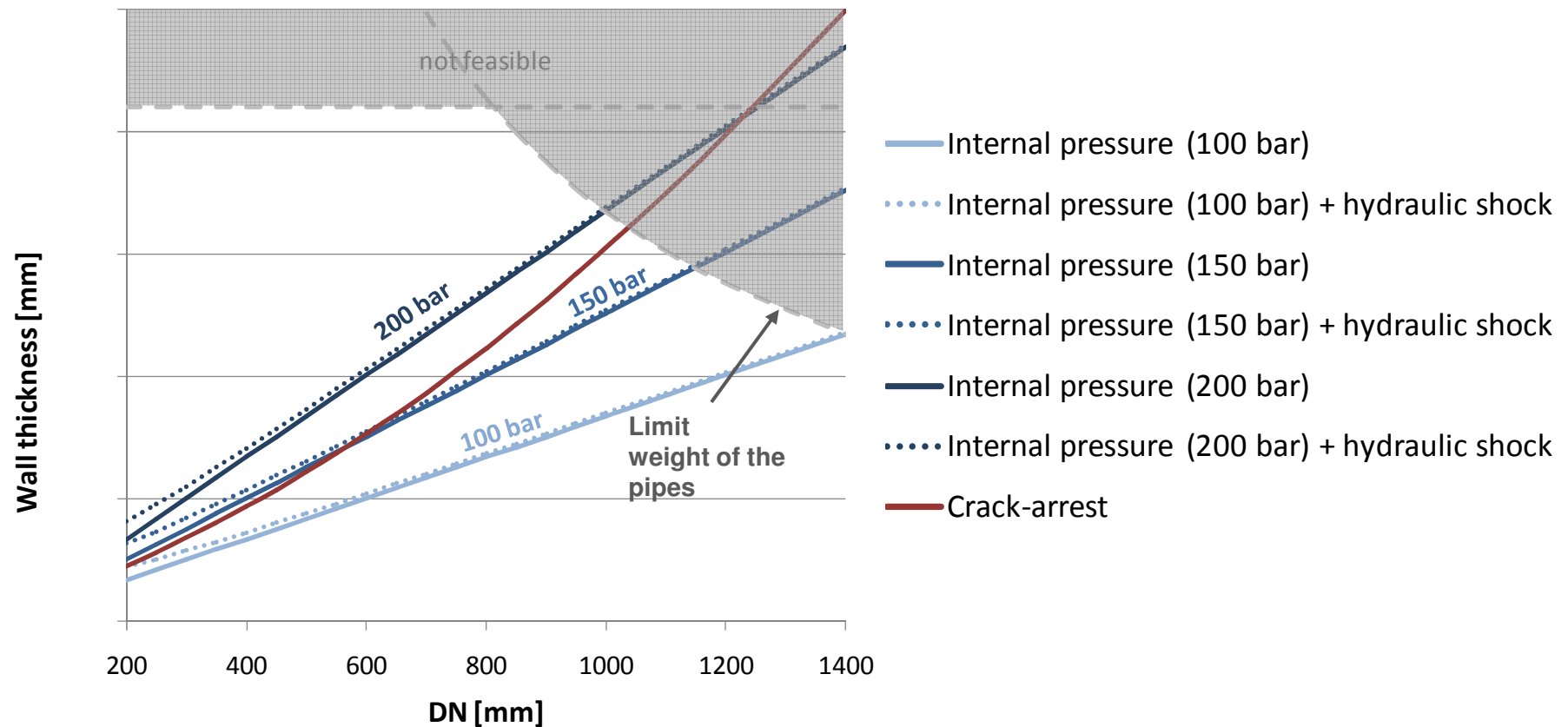
Parameters: Steel X 70, $C_v > 100$ J
Driving pressure at critical point

Calculation of wall thickness

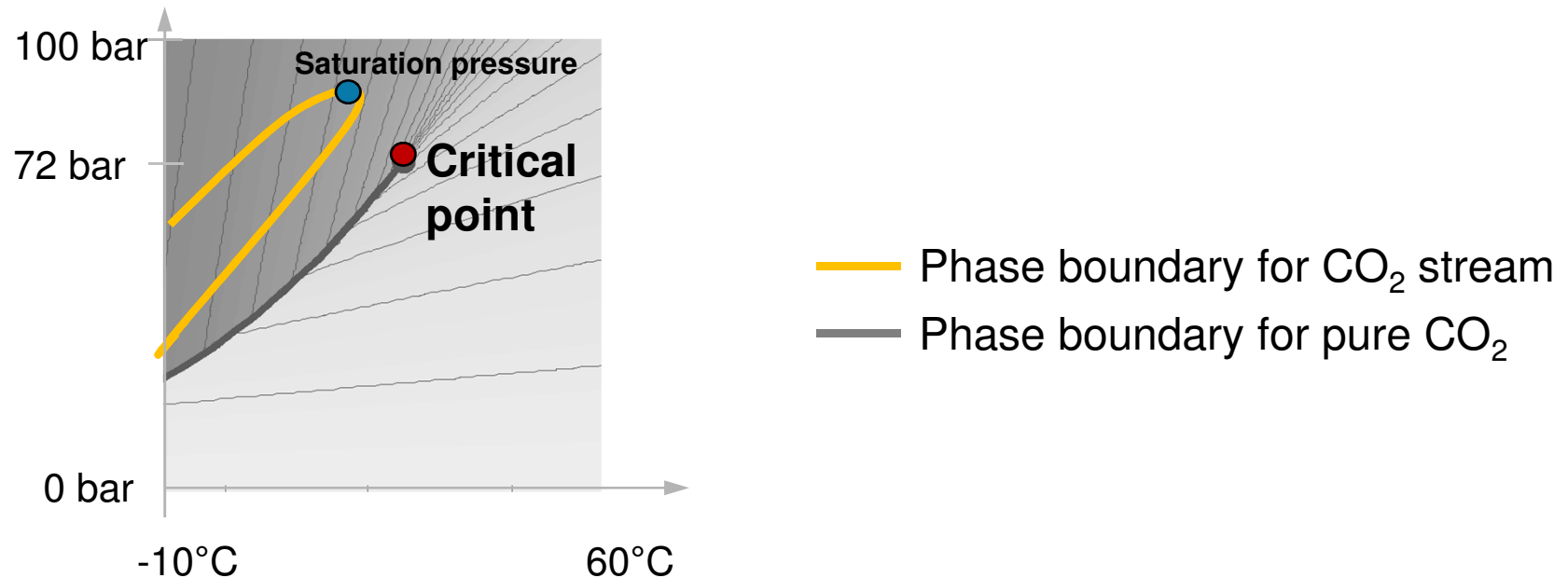
$$T_{min} = \max(T_{minDP}, T_{minHS}, T_{minCA})$$

T_{min} :	Minimum wall thickness
T_{minDP} :	Minimum wall thickness against internal pressure
T_{minHS} :	Minimum wall thickness against hydraulic shock
T_{minCA} :	Minimum wall thickness to assure crack-arrest (which is a function of CO ₂ stream composition)

Minimum wall thickness

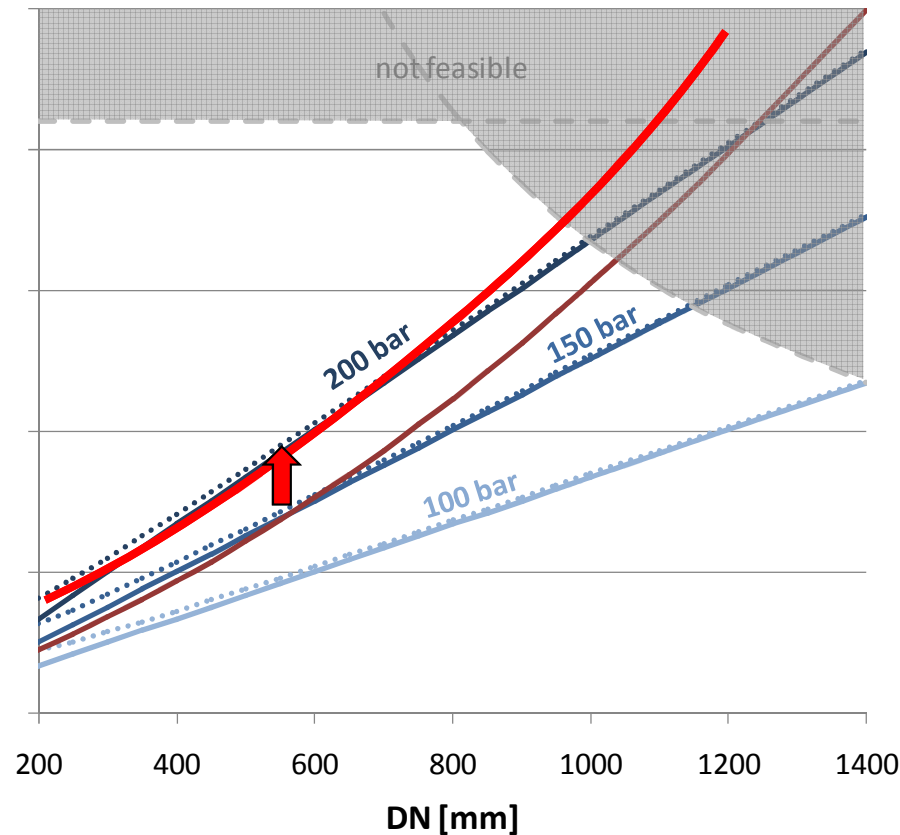


Thermodynamic properties: CO₂ stream with impurities

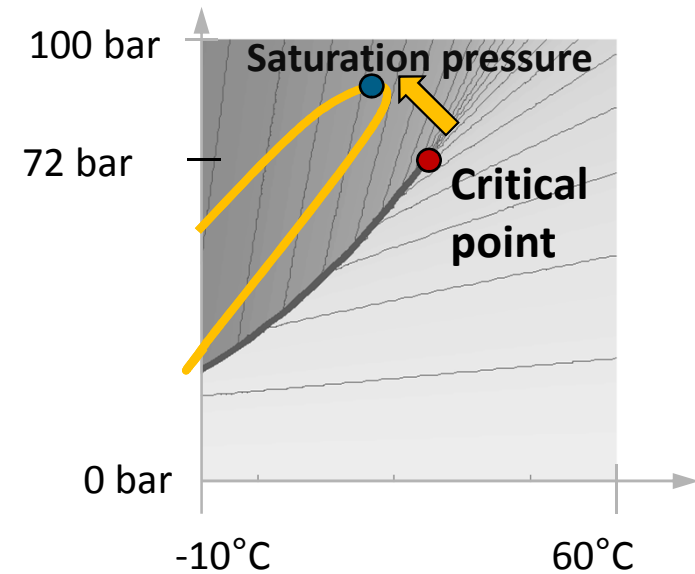


- **The CO₂ composition determines the required wall thickness, what has to be considered in the design phase or limits the operational window.**
- Impurities have impact on thermodynamic properties of a CO₂ stream which cannot be predicted out of the properties of pure CO₂
- Impurities can effect corrosive or generate chemical reactions
- Further properties of a CO₂ stream, like viscosity can change

More wall thickness for crack-arrest for CO₂ streams with impurities



- Wall thickness for CO₂ stream
- Wall thickness for pure CO₂



- Phase boundary for CO₂ stream
- Phase boundary for pure CO₂

Pure CO₂, CO₂-streams with impurities

Pure CO₂, CO₂ streams with impurities have significant consequences on design, construction and operation, e.g.:

Design:

- internal pressure, hydraulic shock and fracture arrest

Construction:

- pipeline bending, pipeline welding

Operation:

- operational envelope

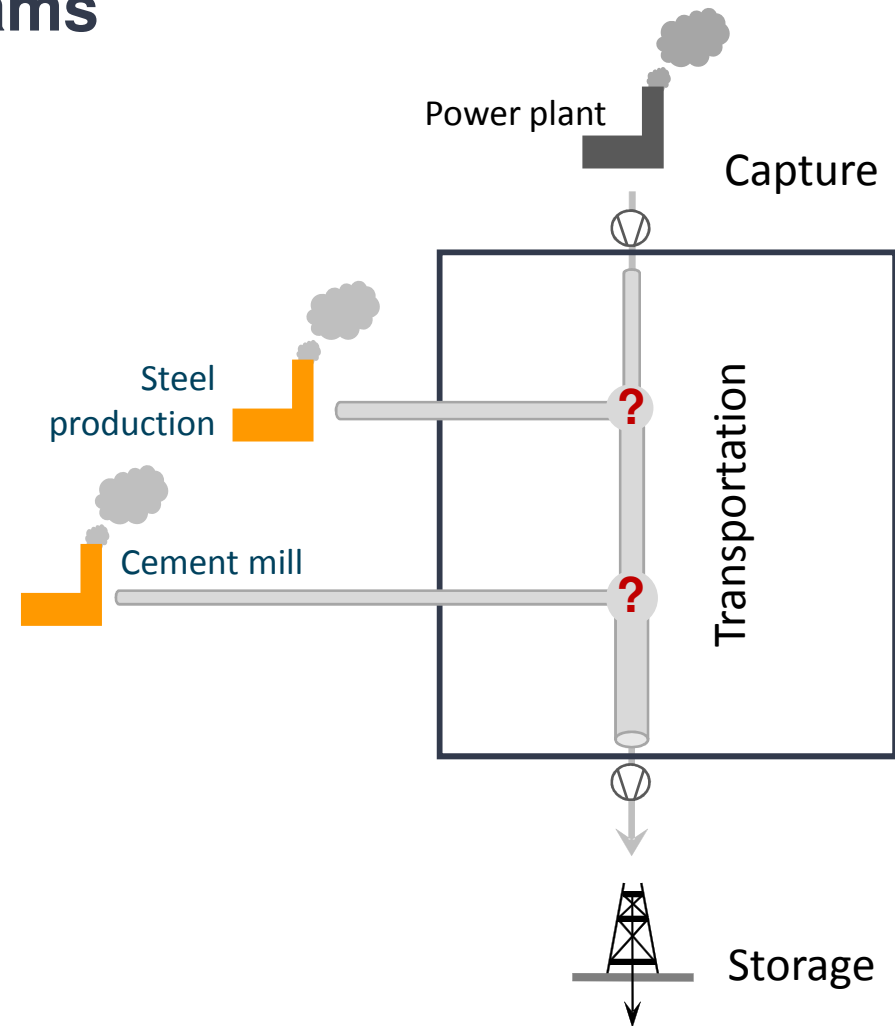
All that has consequences to:

- Fracture arrest design
- Corrosion protection
- Operational window
- Avoidance of two phase flow

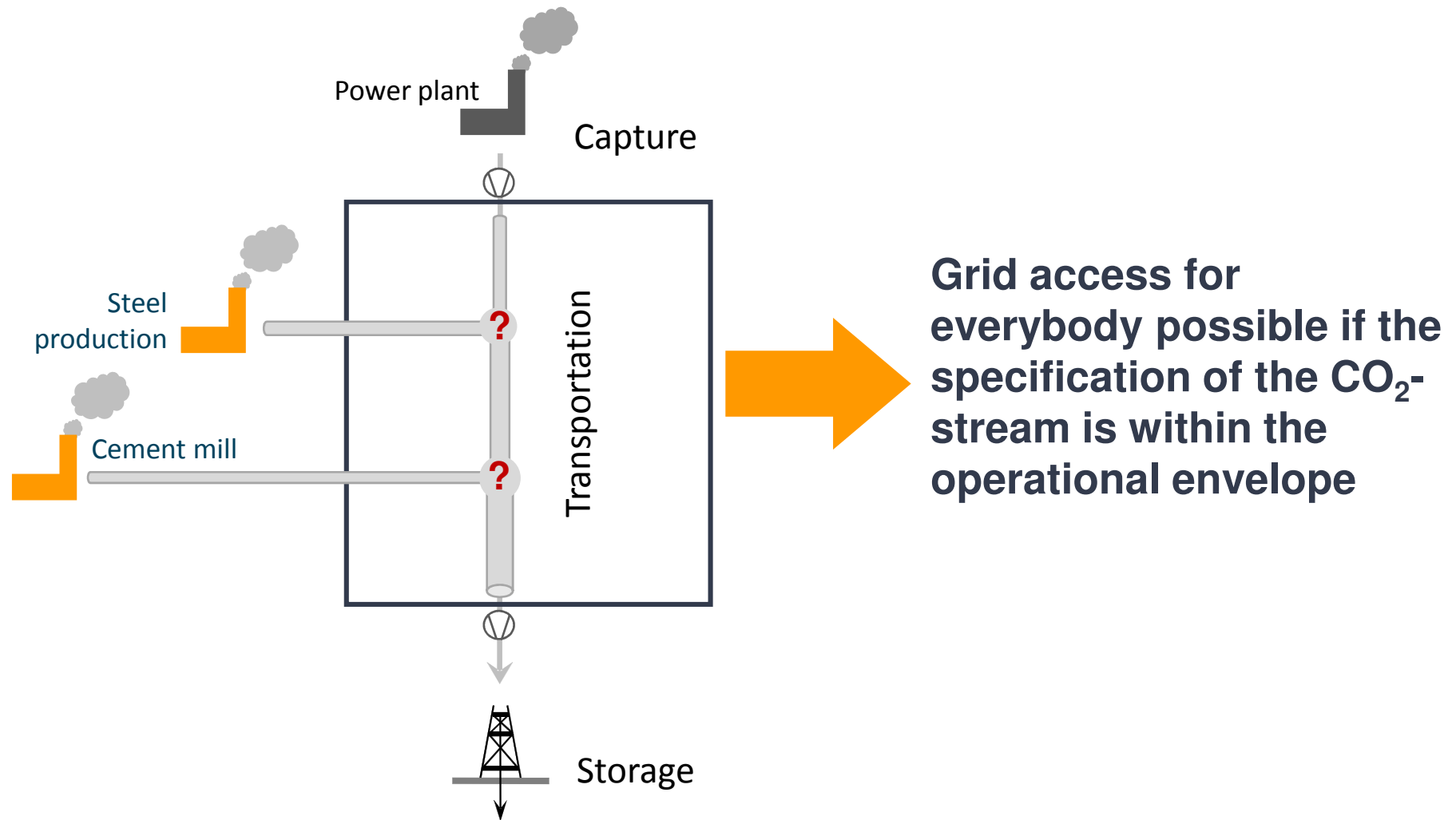
Mixture of different CO₂ streams

In case of mixing of different CO₂ streams in a pipeline network, it must be assured that the mixture of the individual compounds from the different CO₂ streams do not cause:

- Risk of corrosion
- Undesired cross chemical reactions /effects



Grid access and implications for design and operation

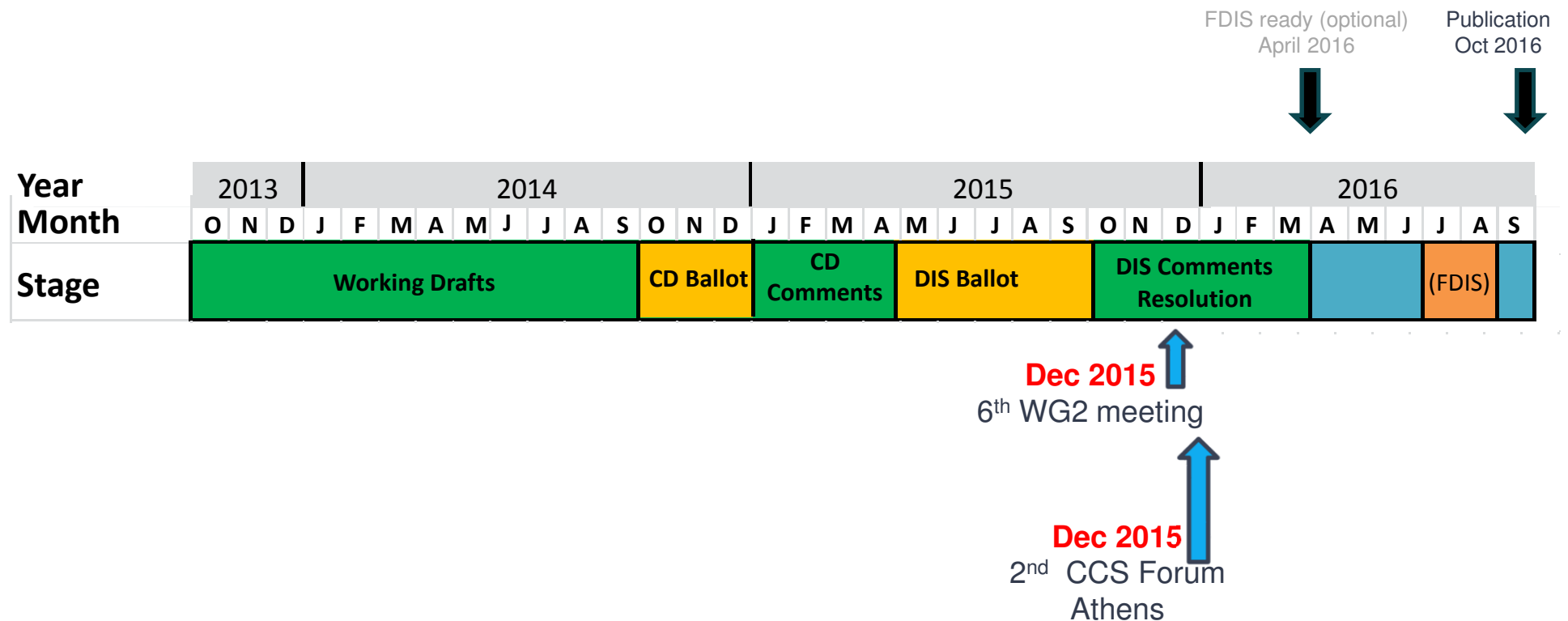


Internal corrosion

- CO₂ pipelines should be designed for corrosion to be within design margins under normal operational conditions.
- For upset conditions a corrosion management plan shall be developed as part of the design. Its scope shall include a plan to recover from failure of the control. Failures can occur upstream of or within the pipeline system.
- For additional information see
Annex C – Internal corrosion (informative)
 - C.1 Measures to minimise internal corrosion
 - C.2 Impact of impurities on internal corrosion
 - C.3 Internal corrosion control

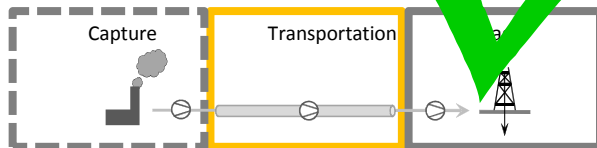


Current status and publication date of Standard



Main Issues

Boundaries to Capture and Storage



(state of the art) Fracture arrest

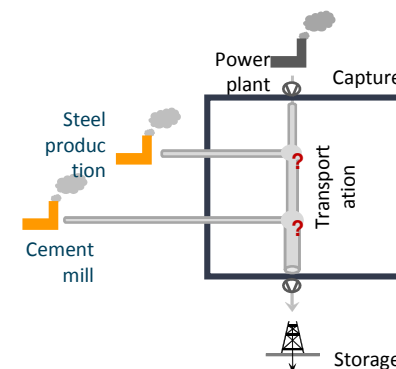


Corrosion



(state of the art)

Non-discriminatory transportation




Summary

- Efficient collaboration on international basis
- Active international participation in the standard development assures broad agreement
- Standard ISO 27913 gives a good framework for design, construction and operation of CO₂ pipelines
- The CO₂ Standard is a valuable supplement to existing Standards for Natural Gas
- This ISO describes the **state of the art** – but **state of the art will develop** in future

Acknowledgement

- Convenor expressed his appreciation

to  for financing the work in 2012 – 2014 and

to  for financing the work in 2015

- Secretary expressed her appreciation

to  for financing the work in 2012 – 2015

Contact:

Dr. Achim Hilgenstock

Hoonkesweg 36

D-46286 Dorsten

Tel +49 2866 17 127

Fax +49 2866 17 125

Mob +49 173 64 88 123

ac@hilgenstock-consulting.de

www.hilgenstock-consulting.de



**Thank you for your
attention**

Back up

Dr.-Ing. Achim Hilgenstock

Education

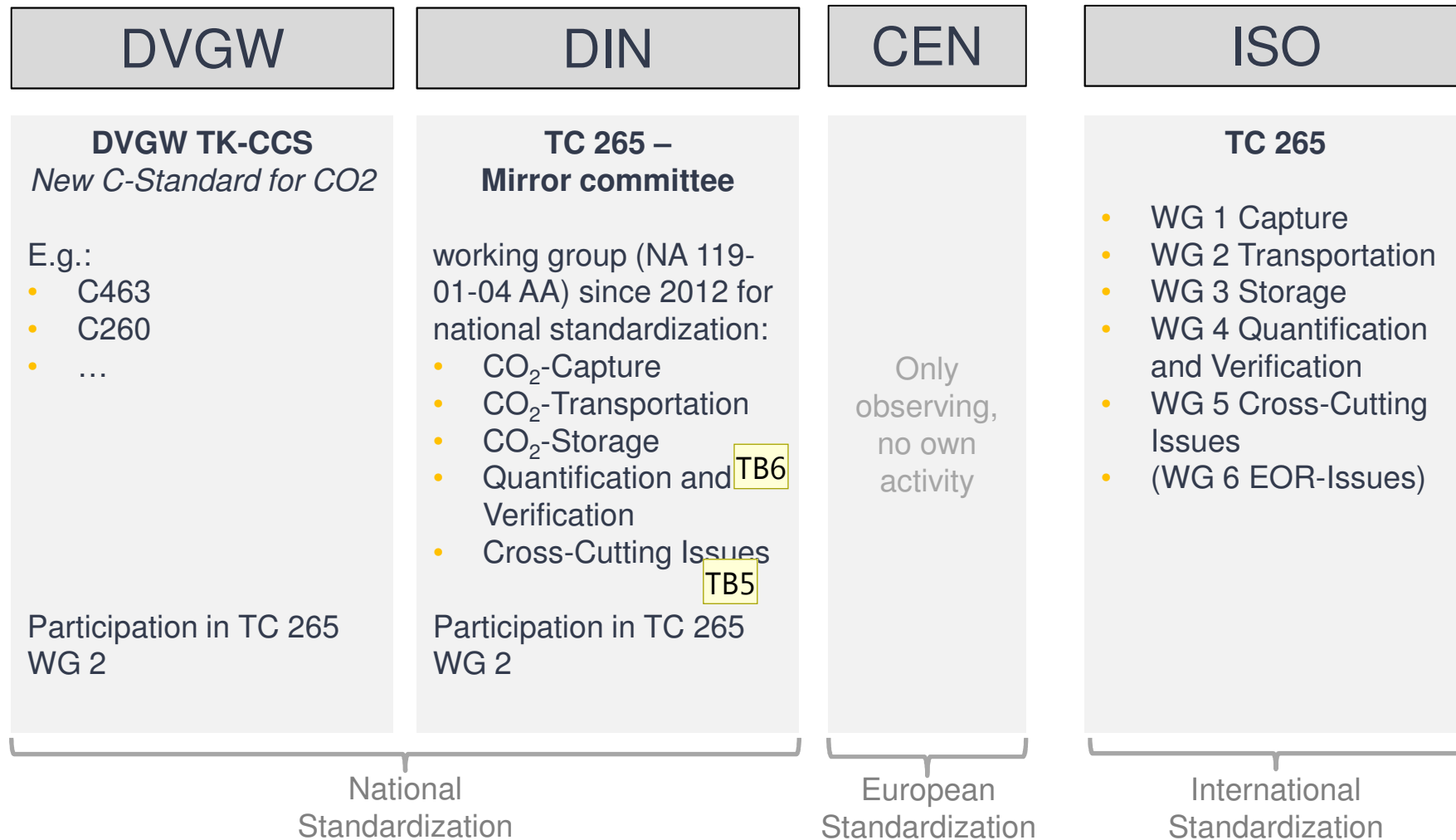
- Mechanical Engineering Ruhr-University Bochum, Germany and Texas A&M University, USA
- Doctoral thesis DLR – Göttingen, University Karlsruhe, Germany

Professional Experience

- 2015 - Consultant Dr. Hilgenstock Consulting
- 2012 - Convenor for ISO/TC 265/WG 2 CO₂ Transportation
- 2012 - Convenor of DVGW expert group CCS
- 2012 - Convenor and national representative of the DVGW/DIN mirror group for CO₂ transport
- 2012 – 2014 Head of Gas Technology and Trading Support E.ON SE
- 2010 – 2012 Vice President Technical Cooperation E.ON Ruhrgas AG
- 2007 - 2010 Head of Pipeline Projects E.ON Ruhrgas AG
- 1999 - 2007 Project Manager Pipeline Projects Ruhrgas AG
- 1996 - 1999 Head of Department Numerical Simulation Ruhrgas AG
- 1992 - 1996 Head of Division Industrial Gas Application Ruhrgas AG
- 1986 - 1992 Research Assistant Theoretical Fluid Dynamics DLR



Standardization activities for CCS



TB5 Auf Deutsch: Übergreifende und Querschnittsaufgaben. Soll ich das so übersetzen?

Baumeister; 25.10.2015

TB6 Siehe obiger Kommentar: Bilanzierung und Verifizierung

Baumeister; 25.10.2015